Remote Handled Disposal Enhancement at the Waste Isolation Pilot Plant

Philip Theisen

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REMOTE HANDLED DISPOSAL ENHANCEMENT
AT THE WASTE ISOLATION PILOT PLANT

BY

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B.S. ARCHITECTURAL ENGINEERING

THESIS

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REMOTE HANDLED DISPOSAL ENHANCEMENT
AT THE WASTE ISOLATION PILOT PLANT

By

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B.S. Architectural Engineering, Illinois Institute of Technology, 2013

ABSTRACT

The Waste Isolation Pilot Plant (WIPP) is a deep underground facility for the disposal of Transuranic Defense Waste located in Southeastern New Mexico. Transuranic (TRU) Waste is defined as any radionuclides with an atomic number greater than that of Uranium, has a half-life greater than 20 years, and activity greater than 100 nanocuries. According to the ‘Land Withdrawal Act’ (LWA), WIPP is licensed to dispose of 6.2 million cubic feet of waste.

TRU waste is categorized into two types: Contact Handled (CH) and Remote Handled (RH). CH waste is any waste that does not have a surface dose rate that exceeds 200 mrem per hour; while RH waste is defined as any waste with a surface dose rate greater than 200 mrem per hour.

WIPP’s current emplacement process for disposing of CH waste is to stack in rows along the floor of the underground panel drift. RH waste is emplaced by the borehole method in the ribs (walls) of the mine via a Horizontal Emplacement Machine (HEM).

The primary dilemma presented by the emplacement rates between CH and RH waste is the inefficiency with meeting the Volume of Record specified in the LWA. WIPP is allowed to dispose of 6.2 million CF of TRU waste. The facility is progressing through the disposal panels in the Underground (UG) at a rate in which available real estate for disposal will be filled before the Volume of Record is reached; and in doing so, disrupting the process for shipping hazardous TRU waste off of the generator sites throughout the Department of Energy (DOE) and into a permanent location for long term disposal.

An investigation will be conducted into a more efficient method for disposing of the RH waste from around the DOE Complex with the intent of dedicating a single panel to strictly RH waste. The concept will allow for the better utilization of RH real estate in the UG assisting the solution to meeting the Volume of Record.
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CHAPTER 1: INTRODUCTION

The WIPP is a deep underground repository for the disposal of Transuranic Defense Waste located in Southeastern New Mexico. WIPP belongs to what has been nicknamed the “Nuclear Corridor” of southeastern New Mexico. URENCO’s enrichment facility in Eunice, New Mexico provides fuel for nuclear power utilities and Waste Control Specialists (WCS) in Andrews, Texas provides nuclear power plants with a low level waste facility. WIPP’s focus is to permanently dispose of TRU Waste from around the DOE complex generated during nation’s nuclear weapon defense program beginning in the early 1940’s. WIPP is licensed to permanently isolate the waste in an underground facility 2,150 feet below the surface for the next 10,000 years. TRU Waste is defined as any radionuclides with an atomic number greater than that of Uranium, has a half-life greater than 20 years, and activity greater than 100 nanocuries per gram.

The waste disposed at WIPP is bounded by the requirements per the LWA in terms of Dose Rates and Volume. Due to the complexity of Hot Cell Operations at the Generator Sites, an inefficiency exists between the amount of waste that is need of being disposed and the real estate available in the WIPP UG. The purpose of this project is to establish a methodology for disposing of RH more efficiently; utilizing the existing facility processes and provide shielding calculations that fit within the bounds of Regulations and the elements of the Facility.

HISTORY

In the 1950’s, the National Academy of Sciences proposed the idea of deep geological disposal for long lived radionuclides. The government spent time during the 1960’s researching potential sites around the nation, which eventually narrowed down to Southeastern New Mexico. Exploratory work for WIPP’s repository location began in 1974 with Construction operations taking place from 1982 until 1988. In 1979 Congress authorized WIPP as a Research and Development project for radioactive waste disposal. President Bush signed the LWA of 1992, a bill to allow the transfer public lands belonging to the State of New Mexico to the DOE. After receiving Certification from the EPA and the HWFP issued by the State of New Mexico for the Resource Conservation and Recovery Act (RCRA), WIPP’s opening occurs and receives their first shipment in 1999 from Los Alamos. To date, five of the ten disposal panels in WIPP’s underground have been undergone final closure.

WIPP started to receive waste in 1999; this was strictly CH waste at the time. In 2007, WIPP received its first RH waste. The first panel to dispose of RH waste was Panel 4; the first three were exclusively CH waste. Since then, WIPP has completely filled six of the ten panels; Panels 9 and 10 being located in the main drifts traversing north and south. Panel 7 just began disposal.
GEOLOGY

The geographical region assigned, the Delaware Basin, was chosen as the most suitable form of long term radioactive disposal. The salt, in which the waste is buried at WIPP, provides a range of advantages for disposing of radioactive waste. For starters, Salt is for all intents and purposes, impermeable. The salt basin at WIPP has existed since the Permian Era, 250 million years ago. This fact has provided enough assurance that free flowing ground water will not flow to the waste causing a radioactive effluent. Salt is also considered “self-healing”. This entails the healing of fractures that might be seen in the formation. If a fracture exists, the salt will close (or creep) filling in the cavity and then bond to the adjacent surfaces. This is an important characteristic to WIPP’s operations. The radioactive waste disposed of at WIPP is emplaced into disposal rooms that are isolated by permanent bulkheads, over time the weight of the ground above the rooms will eventually lead to the a permanent encasing of waste to shield it for the 10,000 year timespan.

SALT DEFENSE DISPOSAL INVESTIGATIONS

SDDI were experiments conducted on Defense High Level Waste (DHLW) to better understand the impact of in-drift emplacement of radioactive waste on the salt; particularly the thermal characteristics observed in the salt. These experiments were conducted in specified drifts of WIPP’s UG. Heaters were used to study the thermal properties from in-drift emplacement. This was seen as operationally beneficial compared to the borehole method described above mainly due to the fact that it is more time efficient. The SDDI concluded that the salt may potentially be an excellent medium to dispose of HLW. Modeling has been performed and the development of test plans is still ongoing.

SURFACE FACILITY

The Surface of WIPP comprises of two primary components to perform waste disposal operations: the four shafts and the Waste Handling Building (WHB). The first shaft is the Air Intake Shaft (AIS). This allows a channel for the airflow to the UG to enter. The air is then pulled through the UG facility via the fans located at the top of the Exhaust Shaft (ES). The airflow will then enter a filtration system before exiting into the environment. The SHS was developed to assist in the mining operations of the UG.

When a new panel is mined a salt haul truck will transport run of mine salt (ROM) to the Salt Handling Shaft (SHS) where it will be carried out of the UG. The last shaft at WIPP is the Waste Handling Shaft (WHS) for waste handing operations. Sections 1.6 and 1.7 describe the CH and RH process used at WIPP, part of which is downloading the waste to the UG after unloading from the shipping containers. Once the waste reaches the bottom of the WHS, a forklift or Transporter will retrieve the waste.
UNDEGROUND FACILITY

The WIPP UG facility is split into three sections: shaft pillar area, north experimental area, and waste disposal area. The shaft pillar area is the defined area from which the ground must be protected due to the location of the shafts providing an exit and source of ventilation. The north experimental area is dedicated to research; and the disposal area is made up of eight panels each with 7 rooms that once filled are then segregated by bulkhead closure. Panels 9A and 10A encompass the main drifts and are planned to be filled upon completion of the first eight panels. Figure 1 represents the basic layout of WIPP.

![Figure 1: WIPP Surface and UG Layout](image)

CONTACT HANDLED WASTE PROCESS

The primary waste disposed of at WIPP is solely TRU Waste. These are categorized into two types at WIPP: CH and RH. CH waste is any waste that does not have a surface dose rate that exceeds 200mrem per hour; while RH waste is defined as any waste with a surface dose rate greater than 200mrem per hour. Both sets of waste are received and processed at WIPP within the confinement of the WHB. This facility is split between a CH Bay and RH Bay. The CH Bay provides a confined area to unload a CH package from the shipping containers: Transuranic Packaging Transporter (TRUPACT) II and TRUPACT III. Half Pacts are also a shipping container approved for receipt and is essentially the same as TRUPACT II except transports half as much in a package. From here the packages are then downloaded via the Waste Handling Shaft to the UG. A vehicle known as the Transporter will then deliver the waste package to the disposal room where a forklift will emplace. The containers are disposed of in a honeycomb

3
pattern along the floor of the disposal room. Approximately 96% of the waste at WIPP is CH.

REMOTE HANDLED WASTE PROCESS

RH waste undergoes a different process as seen in Figure 12. The Shipping Cask is brought into the RH Bay of the WHB and processed through what is called the transfer cell to a Facility Cask. Due to the higher levels of radioactive material within the RH Canisters, the only time it is exposed outside of a cask is in the transfer cell which lined with appropriate concrete shielding. Any other time throughout the process, RH waste is contained within a Cask. This Cask reduces the Dose Rate to 200mrem/hr, same as CH, which allows operators to process without additional precautions. The Facility Cask is then downloaded via the Waste Hoist to the underground where it meets the 41 Ton Forklift to be delivered to the disposal room. RH waste is emplaced by the borehole method in the ribs (walls) of the mine via a Horizontal Emplacement Machine (HEM).

REGULATORY REQUIREMENTS

WIPP’s primary regulating body is the DOE. However, other agencies such as NMED and EPA have jurisdiction over WIPP’s operations, administering the HWFP and Certification, respectively. The HWFP drives the WIPP’s ability to dispose of hazardous waste according to RCRA at the state level. WIPP’s Certification verifies that WIPP’s waste disposal regulations are compliant with 40 CFR. Congress requires that WIPP be recertified every five years until the end of its operational lifetime.

In 1992 Congress set forth the LWA, licensing WIPP to dispose of 6.2 million cubic feet of waste. Here CH waste is defined as being less than 200 mrem/hr and RH is greater than 200 mrem/hr but less than 1,000 rem/hr. Only 5% of WIPP’s waste is allowed to be greater than 1,000 mrem/hr.

Before waste operations could commence, WIPP was required to implement a DSA. This is a in depth hazard analysis that describes WIPP’s site, the facility and equipment, the hazard analysis associated with CH and RH accidents, the SSC’s used for controls, and programmatic descriptions.

Other documents important to this project include: the TRAMPAC, and the WAC. The TRAMPAC documents govern all shipments in TRUPACT II’s, Half Pacts, TRUPACT III’s, and RH-72 Type-B shipping containers. The Waste Acceptance Criteria (WAC) defines the criteria for which the National TRU Program (NTP) generator sites can ship waste to WIPP. These two documents assist in defining the contents and construction of the shipping containers.

The RH Safety Analysis Report (SAR) was also referenced; this document, similar to the Design Safety Analysis (DSA), provides a description of the RH-72 Type-B Shipping Container and the Hazard Accident Conditions (HAC) associated with RH waste. The
vital piece of information in this document is the method for deriving the shielding requirements for an RH canister.

CHAPTER 2: IN SCOPE

The primary dilemmas both these methods offer is the inability to meet the Volume of Record specified by the LWA; At WIPP’s current pace, many of the waste panels in the mine will be full before all the Defense TRU Waste around the DOE Complex has been permanently disposed. One cause of this problem is the inefficiency of the borehole method due to the difference of shipment rates between RH and CH waste. Many of the drilled boreholes stay vacant due to the quicker rate of CH floor emplacement compared to the RH emplacement. The LWA specifies that WIPP shall not exceed any more than 5% of the total volume disposed with a surface dose rate higher 100rem per hour. This makes 95% of the waste received by definition CH waste. The process for mining uses the Just-In-Time concept; a panel is mined at the same time the panel previously mined is being used for waste emplacement. This allows the process the most time possible to utilize for disposal before the weight of the salt (or ground above) creeps in too much to the point of collapsing prematurely. The Just-In-Time method allows workers to emplace waste with the least amount of maintenance during emplacement. Once arrays of CH packages are emplaced, the ground behind it is unable to be maintained. Within the disposal panel RH boreholes are drilled in one room, RH waste canisters are emplaced within the previous room, and CH waste is emplaced in the room previous to RH emplacement. Once again, this utilized the Just-In-Time method to dispose of the waste; but if the process was prolonged to allow for additional RH waste, the rooms would be more difficult to maintain.

The Volume of Record mentioned above, refers to the volume of waste allowed by the LWA to be disposed of at WIPP. This value is based on the volume of containers shipped and not the actual volume of waste packaged in the container. Through radiography, it was discovered that due to the inefficient method of packaging the containers using glove boxes, only about 10% of the containers were being filled with waste. The overarching problem is due to the fact that the CH shipping rates are much quicker than RH and only a small percentage of the waste around the complex is being disposed of, DOE runs the risk of filling up WIPP long before the nation’s laboratories are cleaned up. The following discusses the shipping rates between CH and RH waste per the Supplemental Environmental Impact Statement (SEIS) prepared by DOE.

- CH TRU Waste Rates
  - TRUPACT II Unloading Dock (TRUDOCKS) handling capacity = 50 TRUPACTs/week
  - Assumed 80% efficiency due to worker impact analysis = 40 TRUPACTs/week or 13-14trucks/ week (from SEIS)
- 3 TRUPACTs/Truck
- 3 TRUPACTs fills ~ 2 full positions in disposal room

RH TRU Waste Rates

- 2007-2009 = 2.1/week
- 2009-2010 = 2.8/week
- 2010-2011 = 3.1/week
- 2011-2012 = 1.9/week

RH TRU Borehole Emplacement Rates

- Panel 1-Panel 3 = None
- Panel 4 = 198 boreholes filled
- Panel 5 = 264 boreholes filled
- Panel 6 = 85 boreholes filled
- Total Capacity/Panel = 730 boreholes filled

The floor configuration for emplacing RH canisters was explored by the SDDI. Studied the impact of heat generated from HLW on the surrounding salt. This study will look into the equipment specifications that would support the SDDI concept. The SDDI concluded that using retreat emplacement and horizontally emplaced canisters directly on to the floor using a Remote Operated Vehicle (ROV). The primary focus of this project is the shielding design of that ROV and defining process that the canister will undergo from point of receipt to final disposal. The intent of the conceptual process is to utilize as much of WIPP’s current facilities, equipment and processes as possible.

The goal of this project is to design the shielding of a piece of equipment capable of disposing of RH TRU waste within the geometric parameters of the existing facility and without violating the regulatory bounds that will assist with the overall efficiency towards reaching the volume of record. The conclusion of this project will provide a series of dose calculations and equipment specifications along with a conceptual process.

CHAPTER 3: OUT OF SCOPE

In February of 2014, WIPP experienced two major events: the February 5th fire event and the February 14th Radiological Release. Due to recovery operations, WIPP is not currently open (waste is not being accepted or disposed of). As a result of the accidents, changes are being made to the Safety Basis. Much of the Waste Disposal area in the underground is categorized as Contaminated Areas and Radiation Areas. Panels 9A and 10A are located within these areas as well as the remainder of Panel 7. Currently Panel 8 is the only clean panel and has not been completely mined as of today.

Other items that will not be considered include the process of packaging the waste. As this would provide an alternative solution, the focus of this project will be on the step carried out at WIPP to dispose of the waste in its final resting place.
CHAPTER 4: INITIAL ASSUMPTIONS

The use of a dedicated RH Panel/ Rooms would require under the current conditions of the underground, assuming both CH and RH operations continue, that new panels be mined. This project will not be looking at the alternatives to expanding the mine. It will be assumed that the process used will be operated under a clean environment.

Regarding the Volume of Record, each drum disposed is not full to maximum capacity and hence most of the 6.2 million cubic feet disposed will not be Transuranic Waste. The majority of these drums are made up of approximately 90% air and only 10% waste due to glove box operations. This is a result of the generator site processes and will not be considered in this project.

The waste received at WIPP is required to meet the WAC. This specifies the chemical, radiological, nuclear, and physical limits of the waste being shipped to WIPP. The presumption will be that these limits will not be exceeded and anytime they are, it will be considered an abnormal event.

This design will assume that both the current borehole method and new floor emplacement method will be utilized simultaneously. The floor emplacement method will be reserved for RH waste greater than 100 rem/hr but less than the LWA limit of 1,000 rem/hr. These canisters will be emplaced in a dedicated RH Panel. All waste less than 100 rem/hr (includes both CH and RH) will be disposed of by the same process currently in place at WIPP. The borehole method provides sufficient means to shield the RH Canister from personnel disposing of waste; a new dedicated RH Panel will be a means to dispose of RH with higher Dose Rates in a more efficient way and also relieve the varying rates between CH and RH waste under the current process. The range for the Source Strength will be from 100 rem/hr to 1,000 rem/hr. The process will calculate the thickness required for the Cask needed to reduce the maximum Source limit of 1,000 rem/hr to 200 mrem/hr. The results will then be used to generate the lower Dose Rate with the same thickness but with a Source strength of 100 rem/hr. This will be the Dose Rate range exhibited by the Cask.

CHAPTER 5: METHODOLOGY

The method used for this project will be the Optimization Toolbox in Matlab. The Optimization Toolbox allows for solving functions with a very distinct set of constraints. The solutions can be minimized or maximized based on the intent. Specifically for this project, the optimal objectives include: shielding requirements and equipment specifications.

Before the optimization runs, manual iterations using trial by error will be completed to approximate the range for the independent variable. This independent variable will be
the lead layer. The inner and outer stainless steel layer will be approximated with the manual iterations. The Source strength will be constant; however, after solving for the shielding thickness, a lower Source strength will be used with the same thickness. This will provide the range of Dose rates that will be observed. The buildup factor and mean free path will also vary due to the fact that they are dependent on the thickness.

Since the manual Matlab Iterations provide an approximated range and expected value, the optimization run will provide the exact value needed to obtain a surface dose rate of 200mrem/hr.

CHAPTER 6: CONSTRAINTS

The shielding of the RH equipment allows the waste to be processed as CH. Only when the canister is removed from either the Shipping Cask or Facility Cask does it require a shielded hot cell configuration; which is the transfer cell in this process. The surface dose rate specified by the LWA is 200mrem/hr. The calculations will use a range of shield thicknesses for Lead and Stainless Steel 304 to acquire a dose rate that will then be truncated at 200mrem/hr.

After surface processing, the newly designed cask will download the waste into the mine via the Waste Hoist Shaft. The Waste Hoist is a friction type hoist with a counterweight that is used to raise and lower the conveyance. The conveyance has a 45 ton maximum capacity for RH waste. The new cask design will need to meet both the dose rate limits and the weight capacity; the 8,000 lb loaded canister will be taken into account as well.

Another important bound that needs to be accounted for is the dimensions of the drifts. The Disposal Rooms are approximately 13 feet high, 33 feet wide and 300 feet long. The entrance into the Panel is specified by the DSA as being 14 feet wide. These dimensions will bound the overall turning radii needed by the forklift.

CHAPTER 7: INPUT PARAMETERS

The Shielding Design Calculation will utilize the Dose Rate Equation with a defined set of ranges to generate a Dose Rate. This Dose Rate will then be truncated at the 200 mrem/hr limit.

ENERGY SOURCE

The output of interest for the RH shielding calculations are primarily a dose rate that is within the required limits established by the LWA for both gamma and neutron energies. The energy range specified in the RH-TRU 72-B SAR, will be utilized for the design of the Cask shielding thickness. This range is from 0.1MeV up to 5MeV. All the calculations will be set at the 5MeV bound.
RADIONUCLIDE INVENTORY

Both CH and RH waste received at WIPP are TRU waste from the Cold War Era from around the nuclear production sites. Most of which consists of clothing, tools, rags, residues, debris, etc. Table 1 is an in depth list of the radionuclide inventory as specified by the RH-TRU 72-B SAR. However, the only ten radionuclides comprise of 95% of the radioactive hazard. These are called the Ten WIPP-Tracked Radionuclides as seen in Table 2.

Table 1: WIPP Radionuclide Inventory

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Table 2: Ten WIPP Tracked Radionuclides

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137Cs
SHIELDING MATERIAL

The shielding will comprise of an outer layer of Type 304 Stainless Steel, a layer of Lead, and an inner layer of Type 304 Stainless Steel. The composition and properties of these materials are provided in Table 3 and will be used in the calculation of the mass attenuation coefficients needed for the Mean Free Paths (mfp).

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Table 1: Summary of Shield Regional Densities

SHIELDING THICKNESS

The layers that can be observed in the Clamshell Cask design will include an outer layer of Stainless Steel Type 304, a middle layer of Lead, and an inner layer of Stainless Steel Types 304. The Stainless Steel layers ranged from 1cm, 2cm, 4cm, 6cm, 8cm, and 9cm. The Lead layer was ranged from 0.06cm to 17cm. Only ten Matlab iterations were explored for each Stainless Steel layer to achieve the most accurate solution.

CHAPTER 8: RESULTS

The following illustrates the conceptual design of the equipment and process for the enhancing RH disposal. Both the conceptual designs integrated with the current facility.
and processes at WIPP and the shielding calculations are provided below. The Shielding calculations were also used to derive the dimensions and the net weight of the Cask. These values contributed to the basic capacity and the turning radius of the forklift.

**CLAMSHELL CASKS DESIGN**

The Clamshell Cask (Figure 2) is a shielded transfer device for RH-TR 72-B canisters. Based on the calculations seen in Table 7, the Cask length ranges from 10’-9” to 11’-11”; the canister is 10’ in length. The diameter of the Cask from the Table 7 is an approximate range of 2’-10” to 4’ and the canister has a set diameter of 2’-2”.

The Cask has a Clamshell design is a cylindrical container capable of retracting within itself to allow for access to the inner cavity. The RH Canister will be suspended while the Cask encloses and by doing so encases the Canister. Once in the underground, the Cask opens by the same mechanism as exhibited on the surface except in a horizontal orientation for floor emplacement.

Due to the dimensions of the WHS, the Clamshell Cask will not fit appropriately unto the hoist if placed perpendicularly. The Cask will need the capabilities of rotating 90 degrees for optimal fit. A Clamshell Cask Actuator with a remote gear system will allow for the horizontal rotation of the Cask.

Once delivered to the WHS, the Clamshell Cask poses the issue of rolling. To eliminate rolling, a stabilizing rack (Figure 7) will be utilized on the waste hoist for convenient transporting of the Cask.

![Figure 2: Empty Clamshell Cask Design](image-url)
Figure 3: Loaded Clamshell Cask Design
Figure 4: RH-TRU 72-B Canister Extraction Phase
Figure 5: RH-TRU 72-BCanister Loading Phase
Figure 6: Clamshell Cask Retraction Schematic
Figure 7: Stabilizing Rack Design
SHIELDING PINTEL DESIGN

The RH-TRU 72-B will undergo the same process for horizontal in drift floor emplacement as that of the borehole emplacement up until the loading from the Transfer Cell. The shield bell will be attached to a shielding pintel (Figure 1), which will also be disposable, will be used to grapple the canister and load into the Clamshell Cask. One way lugs will provide the grasping mechanism needed for attaching to the RH canister pintel to pull up into the cask. The shielding pintel will also offer the necessary shielding for the gap. Figure 4 and Figure 5 display the various extraction and loading stages the RH-TRU 72-B Canister will experience in the Transfer Cell and Cask Loading Room.

REMOTE OPERATING VEHICLE DESIGN

An ROV as seen in Figure 4 is the primary piece of equipment that will be used in delivering the Clamshell Cask to its final resting place in the horizontal emplacement process. There will be three separate units needed; one surface unit for transporting the Cask in the Cask Loading Room to the Waste Hoist and two in the Underground; one for transporting the Cask from the Waste Hoist to the RH dedicated Panel airlock and the other to retrieve from the airlock and deliver to its emplacement position.

The forklift apparatus used for lifting the Clamshell Cask will also contain a rotational aspect to allow the Cask to be revolved from the orientation necessary for the RH canister loading to the orientation necessary for placement on the hoist. A vertical rotation allows the Cask to be moved from the loading position to the stabilizing rack in the Waste Hoist. This movement will also be used when retrieving the Cask from the Waste Hoist in the underground. The vertical translation represents the basic mechanism of a forklift in terms of reaching different heights, which will also be needed when staging the Cask on the stabilizing rack. The final orientation that the Cask provides is a horizontal rotation for final disposal on the floor of the RH dedicated room.
Figure 8: ROV
Figure 9: ROV Maneuvering Capabilities

A. Horizontal Rotation  
B. Vertical Rotation  
C. Vertical Translation
SURFACE REMOTE HANDLED PROCESS

As seen in Figure 9, once the RH-TRU 72-B container has been conveyed through the Transfer Cell, the facility grapple will remove the lid of the container and attach to the pintel of the shielding pintel. The shielding pintel will be lowered and permanently attached to the pintel of the RH canister. It is important to note that the shielding pintel is a disposable piece of equipment that will accompany the RH canister for the remainder of its disposal lifetime.

Once the RH canister has been drawn out of the Transfer Cell, the Clamshell Cask will close around the canister as a remote operation. The HEM will approach the Cask and will slide the forks into the fork holes located on the Clamshell Cask Actuator. The Actuator will then rotate the Cask forward until it is in a horizontal alignment. From this position, the forklift will be remotely turned so the Cask can be properly positioned onto the stabilizing rack for transportation down the WHS.

UNDERGROUND REMOTE HANDLED PROCESS

Upon arrival of the Clamshell Cask to the UG via the WHS, an additional ROV will approach the hoist and lift the Cask out of the Stabilizing Rack and off of the hoist. It will then proceed to reverse into the drift and forward towards the RH dedicated panel.

As the ROV reaches the disposal room, the Clamshell Cask Actuator will realign the Clamshell Cask to a perpendicular orientation. The forklift will lower the Cask to the floor while the gear system activates the opening of the outer cask shell. The Clamshell Cask will be emplaced on the floor of the drift and the ROV will reverse out of the room to retrieve additional canisters (Figure 10). The option of stacking the RH canisters will also be available, however not a necessity to the process.

RUN OF MINE SALT PROCESS

After an appropriate amount of RH canisters have been emplaced on the RH dedicated room floor, a remote operated conveyor system with an attached hopper will approach the waste. This hopper will be prefilled with ROM salt by the LHD. The conveyor belt will contain a swiveling end piece for greater range.

The ROM salt will be cascaded onto the RH canisters to provide shielding for a safe work environment for the upcoming shift. These steps will be repeated until the RH dedicated room has been completely filled and closed off (Figure 11).
Figure 10: Surface RH Process
Figure 11: UG RH Process
Figure 12: ROM Salt Shielding Process
Figure 13: RH Processing Flow Chart
DOSE RATE CALCULATIONS

The approach to calculating the surface dose rate seen on the Clamshell Cask was based on a point source within the Canister. This point source allows for a more conservative value as it is making the assumption that the entirety of the radiation is being experienced at a single point adjacent to the inner edge of the cask; as seen in figure 12.

![Figure 14: Point Source Geometry](image)

Both Gamma and Neutron calculations were taken into consideration. For gamma, the isotropic point source dose rate function is Equation 1. Due to the fact that this is a surface dose rate calculation, the Range, R, will simply be the sum of each thickness used in the cask. This is expressed in Equation 2.

\[
D(E) = \frac{S(E)B(E)K(E)}{4\pi R^2} e^{-\chi} \quad \text{Equation 1}
\]

\[
R = \sum t_{pd} + 2t_{ss} \quad \text{Equation 2}
\]

The Dose Rate, D(E), will be the final value of interest and will be truncated at 200mrem/hr as per the LWA. The Source, S(E), will be varied at two dose rates that would be seen on the Canister within the Clamshell Cask. Per the LWA, the maximum
surface dose rate the can be experienced by RH waste is 1,000,000 mrem/hr. The LWA also specifies that only a 5% by volume may be greater than 100,000 mrem/hr. The remaining 95% needs to be greater than 200 mrem/hr but less than the 100,000 mrem/hr. The current borehole method of disposal will still be utilized but restricted to the 95% bin of waste and the process explored for this project will be exclusively for the upper range. The 5% bin will represent the range for the calculations demonstrating a conservative approach with the 1,000,000 mrem/hr and the most efficient approach possible with the 100,000 mrem/hr.

The Build-Up Factor, B(E), is determined from the Geometric Progression function from the ANSI/ANS 1991. Equation 3 and Equation 4 represent the Buildup Factor; Equation 5 is the K_x factor for used in determining the correct Build-Up Factor equation.

\[
B(E) = 1 + (b - 1) \frac{(k^x - 1)}{k - 1}, \quad \text{for } K \neq 1 \quad \text{Equation 3}
\]

\[
B(E) = 1 + (b - 1)x, \quad \text{for } K = 1 \quad \text{Equation 4}
\]

\[
K_x = c x^a + d \frac{(\tanh \frac{x}{2} - 2 - (\tanh(-2)))}{1 - \tanh(-2)}, \quad \text{Equation 5}
\]

The Build-Up Factor is predominantly is for deep penetrations, particularly for mean free paths greater than 20. The Iron Exposure Build-Up Factor Coefficients for a, b, c, d, and K_x are listed in Table 3. For conservative purposes, the Build-Up Factor will assume Lead to be the primary source of shielding; therefore, Table 3 only includes Leads Iron Exposure Coefficients.

It was determined that for all the mean free path’s, K_x yielded a value not equal to one; therefore, Equation 4 was omitted from all calculations in Matlab. Table 3 demonstrates this using the values from Table 4. The mfp’s used were derived from the coding calculations provided through Matlab.
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Table 4: K_x Determination
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Table 4: Kx Determination (Continued)
The Mean Free Paths, $x$, consists of the sum of attenuation coefficients per partial densities and multiplied by the thickness; therefore, $\mu_{\text{Pb}}$, $\mu_{\text{Si}}$, $\mu_{\text{Cr}}$, $\mu_{\text{Mg}}$, $\mu_{\text{Fe}}$, and $\mu_{\text{Ni}}$ are the attenuation coefficients for Lead, Silicon, Chromium, Manganese, Iron, and Nickel respectively. The partial densities are also $\rho_{\text{Pb}}$, $\rho_{\text{Si}}$, $\rho_{\text{Cr}}$, $\rho_{\text{Mg}}$, $\rho_{\text{Fe}}$, and $\rho_{\text{Ni}}$. Equation 6, Equation 7, and Equation 8 list the mfp and the attenuation coefficient for lead and Stainless Steel Type 304. Table 4 contains the material densities, and present of composition, $C$, for Stainless Steel Type 304 and for Lead. The Cask will be designed with an outer layer of Stainless Steel Type 304, a layer of Lead, and an inner layer of Stainless Steel Type 304. Table 5 lists the mass attenuation coefficients for the different elements observed throughout the layers of the shielding.

$$x = \sum \mu_{\text{Pb}} t_{\text{Pb}} + 2 \mu_{\text{SS}} t_{\text{SS}}$$  \hspace{1cm} \text{Equation 6}$$

$$\mu_{\text{SS}} = \frac{\mu_{\text{Si}}}{\rho_{\text{Si}}} C_s + \frac{\mu_{\text{Cr}}}{\rho_{\text{Cr}}} C_{\text{Cr}} + \frac{\mu_{\text{Mg}}}{\rho_{\text{Mg}}} C_{\text{Mg}} + \frac{\mu_{\text{Fe}}}{\rho_{\text{Fe}}} C_{\text{Fe}} + \frac{\mu_{\text{Ni}}}{\rho_{\text{Ni}}} C_{\text{Ni}}$$  \hspace{1cm} \text{Equation 7}$$

$$\mu_{\text{Pb}} = \frac{\mu_{\text{PP}}}{\rho_{\text{Pb}}} C_{\text{Pb}}$$  \hspace{1cm} \text{Equation 8}

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Table 5: Iron Exposure Build-Up Factors. ANSI/ANS 6.4.3-1991
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Table 6: Mass Attenuation Coefficients. ANSI/ANS 6.4.3-1991

The Gamma-Flux-to-Dose Rate Conversion Factor, K(E), provides a conversion when the activity in the canister is known. For these calculations, the constraints will be bound by the limits provided in the LWA; therefore, the Gamma-Flux-to-Dose Rate Conversion Factor will not be applied due to the fact that the source is in unit’s mrem/hr.

The following code summarizes the manual test iterations through Matlab to achieve a Surface Dose Rate by using matrices to establish the varying ranges for the thickness of both Lead and Stainless Steel Type 304.

**MATLAB ITERATION’S RESULTS**

Appendix A provides the various iterations used to calculate the shielding requirements through trial and error in order to reduce the range of the different shielding layers. Each iteration varied the stainless steel type 304 thickness and the range for the lead thickness. Ten values of Lead were calculated for each value of Stainless Steel. The results provided are the dose rates that each corresponding lead thickness. Iterations 1-10 were for a Stainless Steel thickness of 1cm; Iterations 11-20 were for 2cm, Iterations 21-30 were for 4cm, Iterations 31-40 were for 6cm, Iterations 41-50 were for 8cm, and Iterations 51-60 were for 9cm. The last Iteration was generated to provide a more accurate estimation based on the lowest Cask weight that still met the 200 mrem/hr limit.
Figure 15: Dose Rate vs Lead Thickness
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Table 10: Clamshell Cask Specification Results (Continued)
MATLAB OPTIMIZATION RESULTS

After plotting the formula dose rate vs shielding thicknesses, it was concluded that a single local minimum does not exist. The plot below shows that a series of solutions exist along the edge of the surface area representing Dose Rate observed for each configuration of shielding. The solution to Iteration 61 found was validated against the optimization formula generated. Due to the fact, that this solution provided the most acceptable value for fitting the weight limits presented by the Facility, the Shielding Specifications will utilize this value.

![Optimization Plot](image)

Figure 16: Optimization Plot

REMOTE OPERATED VEHICLE LIFTING CAPACITY

Based on the information derived from the Matlab Iterations, it was determined that the ideal weight of the cask that still provided sufficient shielding was 39,095 lbs (19.55 tons) and a height of 134 inches (11'-10'’). Equation 9 demonstrates the specifications needed for the forklift used on the surface and UG facility. The calculations associated with Figure 13 generate an estimated forklift capacity. This capacity is based on the Clamshell Cask being within the bounds of the limits for the Waste Hoist conveyance, which is 45 tons. The RH-TRU 72-B Canister is specified as 4 tons. The values in the
calculations are estimated dimensions of the forklift and are conservative to demonstrate a piece of equipment on the largest scale possible without exceeding the geometry of the drifts in the UG and the maximum capacity of the Waste Hoist conveyance. Using the approximated dimensions of the forklift and the values derived from the shielding calculations (weight and height) the forklift basic capacity was found to be 119 tons. Due to the fact that three total units, 1 surface and 2 underground ROV’s, the forklift will not be loaded onto the Waste Hoist at any point during the operation. Therefore, only the weight of the Cask, Canister, and stabilizing rack contribute to the weight applied to the conveyance. Due to the fact that these geometric specifications were conservatively approximated, the forklift is oversized. However, the weight of the ROV will be much lighter since the counterweight accounts for a portion of the total basic capacity.

Figure 17: ROV Elevation View

\[ Cask\ Weight = \frac{A(B+C)-D(E+F)}{E+G+H} \]  

Equation 9

A= Forklift (Basic Capacity)
B= 2’ (Distance from front wheel center line to fork face)
C= \(x/2+E-B\) (Distance from fork face to rated load center)
D= 0.5 tons (Weight of attachment)
E= 4’ (Distance from front wheel center line to carriage face)
F= 1’ (Distance from carriage face to attachment’s center of gravity)
G= 1’ (Distance from carriage face to rear face of load)
H= \(x/2\) (Distance from rear face of load to center of load)
REMOTE OPERATED VEHICEL TURNING RADIUS

Another specification important to the operation is the turning radius. The geometry of the drifts is sized in such a way that it can support the weight of the salt layers above. Based on the diameter of the shafts, each shaft is provided a shaft pillar. This is the radius in which an only 17% of the ground may be mined in order to protect your egress routes. Outside of these radii,

The Underground mine consists of three total facilities: Shaft Pillar Facility, North Experimental Facility, and Disposal Facility. Both CH and RH are downloaded via the Waste Hoist Shaft; they are then transported through the Shaft Pillar Facility to the Disposal Facility where the Disposal Panels are located. Each panel consists of seven Rooms with dimensions of 13 feet high, 33 feet wide, and 300 feet in length. As seen in Figure 10 and Figure 11, the Canisters will be emplaced using the horizontal emplacement method. WIPP’s DSA has determined that for borehole drilling the minimum spacing for the RH-TRU 72-B Canisters is 30 inches and is not to exceed 10 Kilowatts per acre. The typical spacing is actually eight feet center-to-center.

The Disposal Panel will be dedicated exclusively to RH floor emplacement. The borehole method will be utilized for RH Canisters closer to the 200mrem/hr limit, while the floor emplacement method will be for Canisters approaching the 1,000,000mrem/hr limit. Since the process is hindering on the RH dedicated panel be used solely for higher dose rates, the Disposal Panels will need to posted as High Radiation Areas (HRA) with the operations being conducted remotely. An airlock at the entry of each Panel will be provided along with a staged Stabilizing Rack. This will allow for the transfer of the Clamshell Cask from a ROV on the clean side to drop off the Canister and have a ROV dedicated to the HRA operations. Both ROV’s will need the capability to navigate through the narrow drifts of the underground. Entry ways into the Disposal Panels are typically narrowed to 14 feet wide but expand once the Panel Room has been entered. The turn radii will be based on the fact that Room 1 of a Panel is the immediately after the entrance to a Panel. Therefore the 14 foot limit will be used as the initial drift width followed by a 90 degree turn directly into the 33 foot wide Room. In order to appropriately make these turns in the underground crosscuts (intersections), the ROV will be provided with negative four wheel steering capabilities. The turn radii for each wheel with a maximum deflection angle, δ, of 25°, which yields a maximum turn radius of 19.8° for the outer wheels based on the geometry of the drifts. The length, L, was estimated off of the maximum turn radius and the width of the drift assuming a minimum driving distance between the ROV and Rib (technical term for drift wall) is 1′- 1”. This was figured from the distance in space between the width of the Rib and the length of the Cask as specified in Equation 15. This yielded an axle-to-axle length of 13 feet using Pythagorean's theorem, Figure 14.
\[ R_{IF} = \frac{L}{\sin \theta_{IF}} \]  
\[ R_{OF} = \frac{L}{\sin \theta_{OF}} \]  
\[ R_{IR} = \frac{L}{\sin \theta_{IR}} \]  
\[ R_{OR} = \frac{L}{\sin \theta_{OR}} \]  
(Equation 10)  
(Equation 11)  
(Equation 12)  
(Equation 13)

\[ D = \sqrt{2w_1^2} \]  
(Equation 14)

\[ W_2 = W_1 - W_{\text{Cask}} \]  
(Equation 15)

\( \delta = 25^\circ \)  
(Angle of Deflection)

\( \theta_{IF} = 30^\circ \)  
(Inner Front Wheel Turn Angle)

\( \theta_{OF} = 25^\circ \)  
(Outer Front Wheel Turn Angle)

\( \theta_{IR} = 30^\circ \)  
(Inner Rear Wheel Turn Angle)

\( \theta_{OR} = 25^\circ \)  
(Outer Rear Wheel Turn Angle)

\( W_1 = 14' \)  
(Width of Disposal Panel Rooms)

\( W_2 = W_1 - D_2 \)  
(Width of ROV)

\( W_{\text{Cask}} = 11' - 10'' \)  
(Length of Cask)

\( D_1 = 19' - 9.6'' \)  
(Maximum Turn Radius)

\( D_2 = \frac{(W_1 - W_{\text{Cask}})}{2} \)  
(Approximate Driving Distance from Rib)

\( R_{IF} \)  
(Inner Front Wheel Turn Radius)

\( R_{OF} \)  
(Outer Front Wheel Turn Radius)

\( R_{IR} \)  
(Inner Rear Wheel Turn Radius)

\( R_{OR} \)  
(Outer Rear Wheel Turn Radius)

\( L \)  
(Axle-to-Axle Distance)
CHAPTER 9: CONCLUSION

The purpose of this project was to design an ROV capable of applying the in-drift emplacement method at the WIPP to enhance RH disposal program and help improve the efficiency in utilizing as much of the volume of record as possible. This would require a clamshell cask that is of sufficient thickness to reduce the 1,000,000 mrem/hr maximum limit for acceptable RH waste to 200 mrem/hr. This allows operators to process the cask as a CH, reducing the need for additional changes to the facility’s controls. The cask provides an adequate control from the exchange point between the shipping cask and the clamshell cask, all the way to the final step of in-drift emplacement.

By establishing an RH dedicated panel, in-drift emplacement will be possible since the panel can be bounded as an HRA; only remote operations will be able to be conducted within these bounds. The dynamic movement of the ground will also be easier to maintain if an RH panel is created. Operations can use a Just in Time methodology with the CH waste, mining one panel ahead of the emplacement panel. The same can be applied with an RH dedicated panel.

The shielding calculations provided for the Clamshell Cask were constrained to the regulatory limits as well as the allowable weight on the WHS and the geometry of the
drifts. This resulted in a Clamshell Cask length and weight from the minimum thickness required. For meeting the 200 mrem/hr limit, a thickness of 18cm and 0.1216cm were found for Stainless Steel types 304 and Lead, respectively. These values produced an overall thickness of 18.1216cm (7.1345 in). This also resulted in an overall weight of 31,905 lbs empty and 39,905 lbs loaded; equivalent to 19.55 tons. This is well below the WHS limit of 45 tons.

The ROV was also provided with negative four wheal steering. With this capability, maneuvering through the drifts of the UG will not be an issue. The narrowest drift is 14’ at the entrance to a panel. The length of the Clamshell Cask was found to be 11’-10”. These dimensions were found to be of no hindrance to the ROV’s maneuverability.

Overall, it was concluded that the designs specified will satisfy the constraints that bounded the problem and were also within the required limit. Furthermore, the process utilizes as much of the existing facility so as to reduce the impact on the current waste operations. The process also supports the SDDI concept of in-drift emplacement by an ROV, providing the WIPP with a capability to dispose of CH and RH waste in a more effective manner.

Continuation of this project would potentially include the evaluation of reducing the energy levels specified in the RH-TRU 72-B SAR to generate a lighter and smaller Clamshell Cask that will allow for additional degrees of freedom within the facilities bounds. This can also potentially be obtained by varying the two Stainless Steel layers from each other. An evaluation can be performed to treat the Stainless Steel configuration independently and observe the difference in dose rate from that of the investigated configuration demonstrated in this project.

The process defined here was meant to provide WIPP with a solution to more efficiently disposing of RH waste and improve the rate at which the Volume of Record is being approached. However, the concept of floor emplacement and utilizing the Clamshell Cask mechanism is something that can be explored at other repositories. This concept provides a safe way of disposing of canisters in a remotely operated environment and overall, improving the nuclear waste problem around the world. Other facilities would have the opportunity to utilize or improve on the cask design to better fit the process of their facility. The results of this project do not reflect DOE’s intentions for the WIPP’s waste operations.
APPENDIX A: MATLAB ITERATIONS

Iterations 1-10

%%%Function
%%%Solve for Dose and truncate at 200mrem/hr.
function [ D ] = Dose(S,B,x,R)
D = (S .* B .* exp(-x))./(4 * pi .* R.^2);

%%% Shielding at 5MeV
%%% Source at 1,000,000 mrem/hr
%%% t_SS = 1cm

>> t_Pb=[8 9 10 11 12 13 14 15 16 17]  %% thickness of lead shielding [cm]
t_SS=1  %% thickness of Stainless Steel Shielding [cm]
u_Pb=4.26e-2  %% Mass Attenuation Coefficient for Lead [cm^2/g]
p_Pb=11.35  %% Density of Lead [g/cc]
C_Pb=1.00  %% Percent Composition of Lead
u_1=u_Pb/p_Pb*C_Pb  %% Attenuation Coefficient for Lead
u_Si=2.96e-2  %% Mass Attenuation Coefficient for Silicon [cm^2/g]
p_Si=0.0801  %% Density of Silicon [g/cc]
C_Si=.01  %% Percent Composition of Silicon
u_2=u_Si/p_Si*C_Si  %% Attenuation Coefficient for Silicon
u_Cr=3.05e-2  %% Mass Attenuation Coefficient for Chromium [cm^2/g]
p_Cr=1.5224  %% Density of Chromium [g/cc]
C_Cr=.19  %% Percent Composition of Chromium
u_3=u_Cr/p_Cr*C_Cr  %% Attenuation Coefficient for Chromium
u_Mg=3.04e-2  %% Mass Attenuation Coefficient for Manganese [cm^2/g]
p_Mg=.1663  %% Density of Manganese [g/cc]
C_Mg=.02  \%\%Percent Composition of Mangense
\[ u_4 = \frac{u_{\text{Mg}}}{p_{\text{Mg}}} \times C_{\text{Mg}} \]  \%\%Attenuation Coefficient for Manganese
\[ u_{\text{Fe}} = 3.14 \times 10^{-2} \]  \%\%Mass Attenuation Coefficient for Iron [cm^2/g]
\[ p_{\text{Fe}} = 5.4487 \]  \%\%Density of Iron [g/cc]
C_{\text{Fe}}=.68  \%\%Percent Composition of Iron
\[ u_5 = \frac{u_{\text{Fe}}}{p_{\text{Fe}}} \times C_{\text{Fe}} \]  \%\%Attenuation Coefficient for Iron
\[ u_{\text{Ni}} = 3.28 \times 10^{-2} \]  \%\%Mass Attenuation Coefficient for Nickel [cm^2/g]
\[ p_{\text{Ni}} = .813 \]  \%\%Density of Nickel [g/cc]
C_{\text{Ni}}=.1  \%\%Percent Composition of Nickel
\[ u_6 = \frac{u_{\text{Ni}}}{p_{\text{Ni}}} \times C_{\text{Ni}} \]  \%\%Attenuation Coefficient for Nickel
\[ u_7 = u_2 + u_3 + u_4 + u_5 + u_6 \]  \%\%Attenuation Coefficient for Stainless Steel
\[ x = u_1 \times t_{\text{Pb}} + 2 \times u_7 \times t_{\text{SS}} \]  \%\%Mean Free Path (mfp)
\[ b = 1.48 \times 10^{-2} \]  \%\%Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991
\[ c = 1.01 \times 10^{-2} \]  \%\%Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991
\[ a = 1.2 \times 10^{-2} \]  \%\%Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991
\[ X = 1.31 \times 10^{-1} \]  \%\%Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991
\[ d = 2.58 \times 10^{-2} \]  \%\%Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991
\[ K = c \times a + d \times \frac{((\tanh(x/X) - 2) - (\tanh(-2)))/(1 - \tanh(-2)))}{\tanh(-2)} \]  \%\%Geometric Progression Approximation
\[ B_E = 1 + (b - 1) \times \frac{((K \times x - 1)}/{(K - 1)}) \]  \%\%Build Up Factor
\[ S_E = 1000000 \]  \%\%Source [mrem/hr]
\[ R = 2 \times t_{\text{SS}} + t_{\text{Pb}} \]  \%\%total thickness of material and range to surface dose rate [cm]
\[ \text{Dose}(S_E, B_E, x, R) \]  \%\%Dose Rate [mrem/hr]
\[ t_{\text{Pb}} = \]
Columns 1 through 8
\[
\begin{align*}
8 & 9 & 10 & 11 & 12 & 13 & 14 & 15
\end{align*}
\]
Columns 9 through 10

16  17

$t_{SS} =
1
$u_{Pb} =
0.0426
$p_{Pb} =
11.3500
$C_{Pb} =
1
$u_{1} =
0.0038
$u_{Si} =
0.0296
$p_{Si} =
0.0801
$C_{Si} =
0.0100
$u_{2} =
0.0037
$u_{Cr} =
0.0305
$p_{Cr} =
1.5224
\( C_{\text{Cr}} = 0.1900 \)
\( u_3 = 0.0038 \)
\( u_{\text{Mg}} = 0.0304 \)
\( p_{\text{Mg}} = 0.1663 \)
\( C_{\text{Mg}} = 0.0200 \)
\( u_4 = 0.0037 \)
\( u_{\text{Fe}} = 0.0314 \)
\( p_{\text{Fe}} = 5.4487 \)
\( C_{\text{Fe}} = 0.6800 \)
\( u_5 = 0.0039 \)
\( u_{\text{Ni}} = 0.0328 \)
\( p_{\text{Ni}} = 0.8130 \)
\[ C_{\text{Ni}} = 0.1000 \]

\[ u_6 = 0.0040 \]

\[ u_7 = 0.0191 \]

\[ x = \]

Columns 1 through 5
\[
0.0682 \quad 0.0720 \quad 0.0758 \quad 0.0795 \quad 0.0833
\]

Columns 6 through 10
\[
0.0870 \quad 0.0908 \quad 0.0945 \quad 0.0983 \quad 0.1020
\]

\[ b = 1.4800 \]

\[ c = 1.0100 \]

\[ a = 0.0120 \]

\[ X = 13.1000 \]

\[ d = -0.0258 \]

\[ K = \]

Columns 1 through 5
\[
0.9915 \quad 0.9921 \quad 0.9927 \quad 0.9933 \quad 0.9938
\]
Columns 6 through 10

0.9944  0.9949  0.9953  0.9958  0.9962

B_E =

Columns 1 through 5

1.0329  1.0347  1.0365  1.0383  1.0401

Columns 6 through 10

1.0419  1.0437  1.0455  1.0473  1.0491

S_E =

1000000

R =

Columns 1 through 8

10   11   12   13   14   15   16   17

Columns 9 through 10

18   19

ans =

Columns 1 through 5

767.7220  633.2044  530.9952  451.5322  388.5440

Columns 6 through 10

337.7794  296.2741  261.9101  233.1418  208.8198

>>
Iterations 11-20

%%Function
%%Solve for Dose and truncate at 200mrem/hr.
function [ D ] = Dose(S,B,x,R)
D = (S .* B .* exp(-x))./(4 * pi .* R.^2);

%% Shielding at 5MeV
%% Source at 1,000,000 mrem/hr
%% t_SS = 2cm
>> t_Pb=[8 9 10 11 12 13 14 15 16 17]  %%thickness of lead shielding [cm]
t_SS=2   %%thickness of Stainless Steel Shielding [cm]
u_Pb=4.26e-2 %%Mass Attenuation Coefficient for Lead [cm^2/g]
p_Pb=11.35   %%Density of Lead [g/cc]
C_Pb=1.00  %%Percent Composition of Lead
u_1=u_Pb/p_Pb*C_Pb  %%Attenuation Coefficient for Lead
u_Si=2.96e-2 %%Mass Attenuation Coefficient for Silicon [cm^2/g]
p_Si=0.0801  %%Density of Silicon [g/cc]
C_Si=.01   %%Percent Composition of Silicon
u_2=u_Si/p_Si*C_Si  %%Attenuation Coefficient for Silicon
u_Cr=3.05e-2 %%Mass Attenuation Coefficient for Chromium [cm^2/g]
p_Cr=1.5224 %%Density of Chromium [g/cc]
C_Cr=.19  %%Percent Composition of Chromium
u_3=u_Cr/p_Cr*C_Cr  %%Attenuation Coefficient for Chromium
u_Mg=3.04e-2 %%Mass Attenuation Coefficient for Manganese [cm^2/g]
p_Mg=.1663  %%Density of Manganese [g/cc]
C_Mg=.02   %%Percent Composition of Manganese
\[ u_4 = \frac{u_{Mg}}{p_{Mg}} \times C_{Mg} \quad \text{Attenuation Coefficient for Manganese} \]

\[ u_{Fe} = 3.14 \times 10^{-2} \quad \text{Mass Attenuation Coefficient for Iron [cm}^2/{g]} \]

\[ p_{Fe} = 5.4487 \quad \text{Density of Iron [g/cc]} \]

\[ C_{Fe} = 0.68 \quad \text{Percent Composition of Iron} \]

\[ u_5 = \frac{u_{Fe}}{p_{Fe}} \times C_{Fe} \quad \text{Attenuation Coefficient for Iron} \]

\[ u_{Ni} = 3.28 \times 10^{-2} \quad \text{Mass Attenuation Coefficient for Nickel [cm}^2/{g]} \]

\[ p_{Ni} = 0.813 \quad \text{Density of Nickel [g/cc]} \]

\[ C_{Ni} = 0.1 \quad \text{Percent Composition of Nickel} \]

\[ u_6 = \frac{u_{Ni}}{p_{Ni}} \times C_{Ni} \quad \text{Attenuation Coefficient for Nickel} \]

\[ u_7 = u_2 + u_3 + u_4 + u_5 + u_6 \quad \text{Attenuation Coefficient for Stainless Steel} \]

\[ x = u_1 \times t_{Pb} + 2 \times u_7 \times t_{SS} \quad \text{Mean Free Path (mfp)} \]

\[ b = 1.48 \times 10^0 \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ c = 1.01 \times 10^0 \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ a = 1.2 \times 10^{-2} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ X = 1.31 \times 10^1 \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ d = -2.58 \times 10^{-2} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ K = c \times x + d \times \left( \frac{\text{tanh}(x/X) - \text{tanh}(-2)}{1 - \text{tanh}(-2)} \right) \quad \text{Geometric Progression Approximation} \]

\[ B_E = 1 + (b - 1) \times \left( \frac{K \times x - 1}{K - 1} \right) \quad \text{Build Up Factor} \]

\[ S_E = 1000000 \quad \text{Source [mrem/hr]} \]

\[ R = 2 \times t_{SS} + t_{Pb} \quad \text{total thickness of material and range to surface dose rate [cm]} \]

\[ \text{Dose}(S_E, B_E, x, R) \quad \text{Dose Rate [mrem/hr]} \]

\[ t_{Pb} = \]

Columns 1 through 8

8 9 10 11 12 13 14 15
Columns 9 through 10

16  17

t_SS =

2

u_Pb =

0.0426

p_Pb =

11.3500

C_Pb =

1

u_1 =

0.0038

u_Si =

0.0296

p_Si =

0.0801

C_Si =

0.0100

u_2 =

0.0037

u_Cr =

0.0305

p_Cr =

1.5224
C_{Cr} = 0.1900
u_3 = 0.0038
u_{Mg} = 0.0304
p_{Mg} = 0.1663
C_{Mg} = 0.0200
u_{4} = 0.0037
u_{Fe} = 0.0314
p_{Fe} = 5.4487
C_{Fe} = 0.6800
u_{5} = 0.0039
u_{Ni} = 0.0328
p_{Ni} = 0.8130
\[ C_{\text{Ni}} = 0.1000 \]
\[ u_6 = 0.0040 \]
\[ u_7 = 0.0191 \]
\[ x = \]
\[
\begin{array}{cccccc}
\text{Columns 1 through 5} \\
0.1065 & 0.1102 & 0.1140 & 0.1177 & 0.1215 \\
\text{Columns 6 through 10} \\
0.1252 & 0.1290 & 0.1327 & 0.1365 & 0.1403 \\
\end{array}
\]
\[ b = 1.4800 \]
\[ c = 1.0100 \]
\[ a = 0.0120 \]
\[ X = 13.1000 \]
\[ d = -0.0258 \]
\[ K = \]
\[
\begin{array}{cccccc}
\text{Columns 1 through 5} \\
0.9967 & 0.9971 & 0.9975 & 0.9979 & 0.9983 \\
\end{array}
\]
Columns 6 through 10

0.9986  0.9990  0.9993  0.9996  0.9999

B_E =

Columns 1 through 5

1.0512  1.0530  1.0548  1.0566  1.0584

Columns 6 through 10

1.0602  1.0619  1.0637  1.0655  1.0673

S_E =

1000000

R =

Columns 1 through 8

12  13  14  15  16  17  18  19

Columns 9 through 10

20  21

ans =

Columns 1 through 5

522.2345  444.0705  382.1131  332.1799  291.3550

Columns 6 through 10

257.5549  229.2591  205.3369  184.9335  167.3929

>>
Iterations 21-30

%%Function
%%Solve for Dose and truncate at 200mrem/hr.

function [ D ] = Dose(S,B,x,R)
D = (S .* B .* exp(-x))./(4 * pi .* R.^2);

%% Shielding at 5MeV
%% Source at 1,000,000 mrem/hr
%% t_SS = 4cm

>> t_Pb=[8 9 10 11 12 13 14 15 16 17]  %%thickness of lead shielding [cm]
t_SS=4   %%thickness of Stainless Steel Shielding [cm]
u_Pb=4.26e-2  %%Mass Attenuation Coefficient for Lead [cm²/g]
p_Pb=11.35  %%Density of Lead [g/cc]
C_Pb=1.00   %%Percent Composition of Lead
u_1=u_Pb/p_Pb*C_Pb  %%Attenuation Coefficient for Lead
u_Si=2.96e-2  %%Mass Attenuation Coefficient for Silicon [cm²/g]
p_Si=0.0801  %%Density of Silicon [g/cc]
C_Si=.01  %%Percent Composition of Silicon
u_2=u_Si/p_Si*C_Si  %%Attenuation Coefficient for Silicon
u_Cr=3.05e-2  %%Mass Attenuation Coefficient for Chromium [cm²/g]
p_Cr=1.5224  %%Density of Chromium [g/cc]
C_Cr=.19  %%Percent Composition of Chromium
u_3=u_Cr/p_Cr*C_Cr  %%Attenuation Coefficient for Chromium
u_Mg=3.04e-2  %%Mass Attenuation Coefficient for Manganese [cm²/g]
p_Mg=.1663  %%Density of Manganese [g/cc]
C_Mg=.02  %%Percent Composition of Manganese
\( u_4 = \frac{u_{\text{Mg}}}{p_{\text{Mg}}} C_{\text{Mg}} \)  \% Attenuation Coefficient for Manganese

\( u_{\text{Fe}} = 3.14 \times 10^{-2} \)  \% Mass Attenuation Coefficient for Iron \([\text{cm}^2/\text{g}]\)

\( p_{\text{Fe}} = 5.4487 \)  \% Density of Iron \([\text{g/cc}]\)

\( C_{\text{Fe}} = 0.68 \)  \% Percent Composition of Iron

\( u_5 = \frac{u_{\text{Fe}}}{p_{\text{Fe}}} C_{\text{Fe}} \)  \% Attenuation Coefficient for Iron

\( u_{\text{Ni}} = 3.28 \times 10^{-2} \)  \% Mass Attenuation Coefficient for Nickel \([\text{cm}^2/\text{g}]\)

\( p_{\text{Ni}} = 0.813 \)  \% Density of Nickel \([\text{g/cc}]\)

\( C_{\text{Ni}} = 0.1 \)  \% Percent Composition of Nickel

\( u_6 = \frac{u_{\text{Ni}}}{p_{\text{Ni}}} C_{\text{Ni}} \)  \% Attenuation Coefficient for Nickel

\( u_7 = u_2 + u_3 + u_4 + u_5 + u_6 \)  \% Attenuation Coefficient for Stainless Steel

\( x = u_1 \cdot t_{\text{Pb}} + 2 \cdot u_7 \cdot t_{\text{SS}} \)  \% Mean Free Path (mfp)

\( b = 1.48 \times 10^0 \)  \% Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991

\( c = 1.01 \times 10^0 \)  \% Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991

\( a = 1.2 \times 10^{-2} \)  \% Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991

\( X = 1.31 \times 10^1 \)  \% Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991

\( d = 2.58 \times 10^{-2} \)  \% Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991

\( K = c \cdot x \cdot a + d \cdot ((\tanh(x/X) - 2) - \tanh(-2)) / (1 - \tanh(-2)) \)  \% Geometric Progression Approximation

\( B_{\text{E}} = 1 + (b - 1) \cdot ((K \cdot x - 1) / (K - 1)) \)  \% Build Up Factor

\( S_{\text{E}} = 1000000 \)  \% Source [mrem/hr]

\( R = 2 \cdot t_{\text{SS}} + t_{\text{Pb}} \)  \% total thickness of material and range to surface dose rate [cm]

\( \text{Dose}(S_{\text{E}}, B_{\text{E}}, x, R) \)  \% Dose Rate [mrem/hr]

\( t_{\text{Pb}} = \)

Columns 1 through 8

8 9 10 11 12 13 14 15
Columns 9 through 10

16 17

t_SS =

4

u_Pb =

0.0426

p_Pb =

11.3500

C_Pb =

1

u_1 =

0.0038

u_Si =

0.0296

p_Si =

0.0801

C_Si =

0.0100

u_2 =

0.0037

u_Cr =

0.0305

p_Cr =

1.5224
\[ C_{\text{Cr}} = 0.1900 \]
\[ u_3 = 0.0038 \]
\[ u_{\text{Mg}} = 0.0304 \]
\[ p_{\text{Mg}} = 0.1663 \]
\[ C_{\text{Mg}} = 0.0200 \]
\[ u_4 = 0.0037 \]
\[ u_{\text{Fe}} = 0.0314 \]
\[ p_{\text{Fe}} = 5.4487 \]
\[ C_{\text{Fe}} = 0.6800 \]
\[ u_5 = 0.0039 \]
\[ u_{\text{Ni}} = 0.0328 \]
\[ p_{\text{Ni}} = 0.8130 \]
C_Ni =

0.1000

u_6 =

0.0040

u_7 =

0.0191

x =

Columns 1 through 5
0.1829 0.1867 0.1904 0.1942 0.1979

Columns 6 through 10
0.2017 0.2054 0.2092 0.2129 0.2167

b =

1.4800

c =

1.0100

a =

0.0120

X =

13.1000

d =

-0.0258

K =

Columns 1 through 5
1.0030 1.0033 1.0035 1.0037 1.0040
Columns 6 through 10
1.0042  1.0044  1.0046  1.0048  1.0050

B_E =

Columns 1 through 5
1.0877  1.0895  1.0913  1.0931  1.0949

Columns 6 through 10
1.0966  1.0984  1.1002  1.1020  1.1038

S_E =
1000000

R =

Columns 1 through 8
16  17  18  19  20  21  22  23

Columns 9 through 10
24  25

ans =

Columns 1 through 5
281.5894  248.9104  221.5538  198.4263  178.7012

Columns 6 through 10
161.7442  147.0620  134.2665  123.0488  113.1605

>>
Iterations 31-40

%%% Function
%%% Solve for Dose and truncate at 200mrem/hr.

function [ D ] = Dose(S,B,x,R)
D = (S .* B .* exp(-x))./(4 * pi .* R.^2);

%%% Shielding at 5MeV
%%% Source at 1,000,000 mrem/hr
%%% t_SS = 6cm

>> t_Pb=[8 9 10 11 12 13 14 15 16 17]  %% thickness of lead shielding [cm]
t_SS=6   %% thickness of Stainless Steel Shielding [cm]
u_Pb=4.26e-2  %% Mass Attenuation Coefficient for Lead [cm^2/g]
p_Pb=11.35  %% Density of Lead [g/cc]
C_Pb=1.00  %% Percent Composition of Lead

u_1=u_Pb/p_Pb*C_Pb  %% Attenuation Coefficient for Lead
u_Si=2.96e-2  %% Mass Attenuation Coefficient for Silicon [cm^2/g]
p_Si=0.0801  %% Density of Silicon [g/cc]
C_Si=.01  %% Percent Composition of Silicon

u_2=u_Si/p_Si*C_Si  %% Attenuation Coefficient for Silicon
u_Cr=3.05e-2  %% Mass Attenuation Coefficient for Chromium [cm^2/g]
p_Cr=1.5224  %% Density of Chromium [g/cc]
C_Cr=.19  %% Percent Composition of Chromium

u_3=u_Cr/p_Cr*C_Cr  %% Attenuation Coefficient for Chromium
u_Mg=3.04e-2  %% Mass Attenuation Coefficient for Manganese [cm^2/g]
p_Mg=.1663  %% Density of Manganese [g/cc]
C_Mg=.02  %% Percent Composition of Manganese
u_4 = \frac{u_{Mg}}{p_{Mg} \cdot C_{Mg}} \quad \text{Attenuation Coefficient for Manganese} \\
u_{Fe} = 3.14 \times 10^{-2} \quad \text{Mass Attenuation Coefficient for Iron} \quad [\text{cm}^2/\text{g}] \\
p_{Fe} = 5.4487 \quad \text{Density of Iron} \quad [\text{g/cc}] \\
C_{Fe} = 0.68 \quad \text{Percent Composition of Iron} \\
u_5 = \frac{u_{Fe}}{p_{Fe} \cdot C_{Fe}} \quad \text{Attenuation Coefficient for Iron} \\
u_{Ni} = 3.28 \times 10^{-2} \quad \text{Mass Attenuation Coefficient for Nickel} \quad [\text{cm}^2/\text{g}] \\
p_{Ni} = 0.813 \quad \text{Density of Nickel} \quad [\text{g/cc}] \\
C_{Ni} = 0.1 \quad \text{Percent Composition of Nickel} \\
u_6 = \frac{u_{Ni}}{p_{Ni} \cdot C_{Ni}} \quad \text{Attenuation Coefficient for Nickel} \\
u_7 = u_{2} + u_{4} + u_{5} + u_{6} \quad \text{Attenuation Coefficient for Stainless Steel} \\
x = u_{1} \cdot t_{Pb} + 2 \cdot u_{7} \cdot t_{SS} \quad \text{Mean Free Path (mfp)} \\
b = 1.48 \times 10^{0} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \\
c = 1.01 \times 10^{0} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \\
a = 1.2 \times 10^{-2} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \\
X = 1.31 \times 10^{1} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \\
d = 2.58 \times 10^{-2} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \\
K = c \cdot x \cdot a + d \cdot \frac{((\text{tanh}(x/X) - 2 - \text{tanh}(-2)))/(1 - \text{tanh}(-2)))}{(K - 1)} \quad \text{Geometric Progression Approximation} \\
B_E = 1 + (b - 1) \cdot ((K \cdot x - 1)/(K - 1)) \quad \text{Build Up Factor} \\
S_E = 1000000 \quad \text{Source [mrem/hr]} \\
R = 2 \cdot t_{SS} + t_{Pb} \quad \text{total thickness of material and range to surface dose rate [cm]} \\
Dose(S_E, B_E, x, R) \quad \text{Dose Rate [mrem/hr]} \\
t_{Pb} =

Columns 1 through 8

8 9 10 11 12 13 14 15
Columns 9 through 10

16  17

t_{SS} =

6

u_{Pb} =

0.0426

p_{Pb} =

11.3500

C_{Pb} =

1

u_{1} =

0.0038

u_{Si} =

0.0296

p_{Si} =

0.0801

C_{Si} =

0.0100

u_{2} =

0.0037

u_{Cr} =

0.0305

p_{Cr} =

1.5224
C_{Cr} = 0.1900
u_3 = 0.0038
u_{Mg} = 0.0304
p_{Mg} = 0.1663
C_{Mg} = 0.0200
u_4 = 0.0037
u_{Fe} = 0.0314
p_{Fe} = 5.4487
C_{Fe} = 0.6800
u_5 = 0.0039
u_{Ni} = 0.0328
p_{Ni} = 0.8130
\[ C_{Ni} = 0.1000 \]
\[ u_6 = 0.0040 \]
\[ u_7 = 0.0191 \]
\[ x = \]
\[ \text{Columns 1 through 5} \quad 0.2594 \quad 0.2631 \quad 0.2669 \quad 0.2706 \quad 0.2744 \]
\[ \text{Columns 6 through 10} \quad 0.2781 \quad 0.2819 \quad 0.2856 \quad 0.2894 \quad 0.2931 \]
\[ b = 1.4800 \]
\[ c = 1.0100 \]
\[ a = 0.0120 \]
\[ X = 13.1000 \]
\[ d = -0.0258 \]
\[ K = \]
\[ \text{Columns 1 through 5} \quad 1.0071 \quad 1.0073 \quad 1.0075 \quad 1.0076 \quad 1.0078 \]
Columns 6 through 10
  1.0079  1.0081  1.0082  1.0084  1.0086

B_E =

Columns 1 through 5
  1.1242  1.1260  1.1277  1.1295  1.1313

Columns 6 through 10
  1.1331  1.1349  1.1367  1.1385  1.1403

S_E =

  1000000

R =

Columns 1 through 8
  20  21  22  23  24  25  26  27

Columns 9 through 10
  28  29

ans =

Columns 1 through 5
  172.5528  156.1725  141.9901  129.6304  118.7949

Columns 6 through 10
  109.2439  100.7828  93.2525  86.5218  80.4819

>>
Iterations 41-50

%%Function

%%Solve for Dose and truncate at 200mrem/hr.

function [ D ] = Dose(S,B,x,R)
D = (S .* B .* exp(-x))./(4 * pi .* R.^2);

%% Shielding at 5MeV
%% Source at 1,000,000 mrem/hr

%% t_SS = 8cm

>> t_Pb=[1 2 3 4 5 6 7 8 9 10]  %% thickness of lead shielding [cm]
t_SS=8  %% thickness of Stainless Steel Shielding [cm]
u_Pb=4.26e-2  %% Mass Attenuation Coefficient for Lead [cm^2/g]
p_Pb=11.35  %% Density of Lead [g/cc]
C_Pb=1.00  %% Percent Composition of Lead
u_1=u_Pb/p_Pb*C_Pb  %% Attenuation Coefficient for Lead
u_Si=2.96e-2  %% Mass Attenuation Coefficient for Silicon [cm^2/g]
p_Si=0.0801  %% Density of Silicon [g/cc]
C_Si=.01  %% Percent Composition of Silicon
u_2=u_Si/p_Si*C_Si  %% Attenuation Coefficient for Silicon
u_Cr=3.05e-2  %% Mass Attenuation Coefficient for Chromium [cm^2/g]
p_Cr=1.5224  %% Density of Chromium [g/cc]
C_Cr=.19  %% Percent Composition of Chromium
u_3=u_Cr/p_Cr*C_Cr  %% Attenuation Coefficient for Chromium
u_Mg=3.04e-2  %% Mass Attenuation Coefficient for Manganese [cm^2/g]
p_Mg=.1663  %% Density of Manganese [g/cc]
C_Mg=.02  %% Percent Composition of Manganese
u_4 = \frac{u_{Mg}}{p_{Mg}} \times C_{Mg}  \quad \%\%\text{Attenuation Coefficient for Manganese}

u_{Fe} = 3.14 \times 10^{-2}  \quad \%\%\text{Mass Attenuation Coefficient for Iron [cm}^2\text{/g]}

p_{Fe} = 5.4487  \quad \%\%\text{Density of Iron [g/cc]}

C_{Fe} = 0.68  \quad \%\%\text{Percent Composition of Iron}

u_5 = \frac{u_{Fe}}{p_{Fe}} \times C_{Fe}  \quad \%\%\text{Attenuation Coefficient for Iron}

u_{Ni} = 3.28 \times 10^{-2}  \quad \%\%\text{Mass Attenuation Coefficient for Nickle [cm}^2\text{/g]}

p_{Ni} = 0.813  \quad \%\%\text{Density of Nickel [g/cc]}

C_{Ni} = 0.1  \quad \%\%\text{Percent Composition of Nickel}

u_6 = \frac{u_{Ni}}{p_{Ni}} \times C_{Ni}  \quad \%\%\text{Attenuation Coefficient for Nickel}

u_7 = u_2 + u_3 + u_4 + u_5 + u_6  \quad \%\%\text{Attenuation Coefficient for Stainless Steel}

x = u_1 \times t_{Pb} + 2 \times u_7 \times t_{SS}  \quad \%\%\text{Mean Free Path (mfp)}

b = 1.48 \times 10^0  \quad \%\%\text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991}

c = 1.01 \times 10^0  \quad \%\%\text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991}

a = 1.2 \times 10^{-2}  \quad \%\%\text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991}

X = 1.31 \times 10^1  \quad \%\%\text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991}

d = -2.58 \times 10^{-2}  \quad \%\%\text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991}

K = c \times x^a + d \times \frac{((\tanh(x/X) - 2) - (\tanh(-2))}{(1 - \tanh(-2))}  \quad \%\%\text{Geometric Progression Approximation}

B_E = 1 + (b - 1) \times \frac{(K \times x - 1)}{K - 1}  \quad \%\%\text{Build Up Factor}

S_E = 1000000  \quad \%\%\text{Source [mrem/hr]}

R = 2 \times t_{SS} + t_{Pb}  \quad \%\%\text{total thickness of material and range to surface dose rate [cm]}

Dose(S_E, B_E, x, R)  \quad \%\%\text{Dose Rate [mrem/hr]}

t_{Pb} =

Columns 1 through 8

1 2 3 4 5 6 7 8
Columns 9 through 10

9    10

t_SS =
8

u_Pb =
0.0426

p_Pb =
11.3500

C_Pb =
1

u_1 =
0.0038

u_Si =
0.0296

p_Si =
0.0801

C_Si =
0.0100

u_2 =
0.0037

u_Cr =
0.0305

p_Cr =
1.5224
\[\begin{align*}
C_{\text{Cr}} & = 0.1900 \\
u_3 & = 0.0038 \\
u_{\text{Mg}} & = 0.0304 \\
p_{\text{Mg}} & = 0.1663 \\
C_{\text{Mg}} & = 0.0200 \\
u_4 & = 0.0037 \\
u_{\text{Fe}} & = 0.0314 \\
p_{\text{Fe}} & = 5.4487 \\
C_{\text{Fe}} & = 0.6800 \\
u_5 & = 0.0039 \\
u_{\text{Ni}} & = 0.0328 \\
p_{\text{Ni}} & = 0.8130
\end{align*}\]
\[ C_{Ni} = 0.1000 \]
\[ u_6 = 0.0040 \]
\[ u_7 = 0.0191 \]
\[ x = \]
\[
\begin{array}{cccccc}
\text{Columns 1 through 5} \\
0.3095 & 0.3133 & 0.3170 & 0.3208 & 0.3245 \\
\text{Columns 6 through 10} \\
0.3283 & 0.3321 & 0.3358 & 0.3396 & 0.3433 \\
\end{array}
\]
\[ b = 1.4800 \]
\[ c = 1.0100 \]
\[ a = 0.0120 \]
\[ X = 13.1000 \]
\[ d = -0.0258 \]
\[ K = \]
\[
\begin{array}{cccccc}
\text{Columns 1 through 5} \\
1.0092 & 1.0093 & 1.0095 & 1.0096 & 1.0097 \\
\end{array}
\]
Columns 6 through 10
1.0099  1.0100  1.0101  1.0103  1.0104

B_E =

Columns 1 through 5
1.1481  1.1499  1.1517  1.1535  1.1553

Columns 6 through 10
1.1571  1.1589  1.1606  1.1624  1.1642

S_E =
1000000

R =

Columns 1 through 8
17  18  19  20  21  22  23  24

Columns 9 through 10
25  26

ans =

Columns 1 through 5
231.9780  206.4651  184.8973  166.5032  150.6912

Columns 6 through 10
137.0011  125.0708  114.6119  105.3931  97.2264

>>
Iterations 51-60

%% Function

%% Solve for Dose and truncate at 200mrem/hr.

function [ D ] = Dose(S,B,x,R)
D = (S .* B .* exp(-x))./(4 * pi * R.^2);

%% Shielding at 5MeV

%% Source at 1,000,000 mrem/hr

%% t_SS = 9cm

>> t_Pb=[0.06 0.07 0.08 0.09 0.1 0.11 0.12 0.13 0.14 0.15]  %% thickness of lead shielding [cm]
t_SS=9  %% thickness of Stainless Steel Shielding [cm]
u_Pb=4.26e-2  %% Mass Attenuation Coefficient for Lead [cm^2/g]
p_Pb=11.35  %% Density of Lead [g/cc]
C_Pb=1.00  %% Percent Composition of Lead

u_1=u_Pb/p_Pb*C_Pb  %% Attenuation Coefficient for Lead

u_Si=2.96e-2  %% Mass Attenuation Coefficient for Silicon [cm^2/g]
p_Si=0.0801  %% Density of Silicon [g/cc]
C_Si=.01  %% Percent Composition of Silicon

u_2=u_Si/p_Si*C_Si  %% Attenuation Coefficient for Silicon

u_Cr=3.05e-2  %% Mass Attenuation Coefficient for Chromium [cm^2/g]
p_Cr=1.5224  %% Density of Chromium [g/cc]
C_Cr=.19  %% Percent Composition of Chromium

u_3=u_Cr/p_Cr*C_Cr  %% Attenuation Coefficient for Chromium

u_Mg=3.04e-2  %% Mass Attenuation Coefficient for Manganese [cm^2/g]
p_Mg=.1663  %% Density of Manganese [g/cc]
C_Mg=.02  %% Percent Composition of Manganese
\[ u_4 = \frac{u_{Mg}}{p_{Mg}} \times C_{Mg} \quad \text{Attenuation Coefficient for Manganese} \]

\[ u_{Fe} = 3.14 \times 10^{-2} \quad \text{Mass Attenuation Coefficient for Iron [cm}^2/\text{g]} \]

\[ p_{Fe} = 5.4487 \quad \text{Density of Iron [g/cc]} \]

\[ C_{Fe} = 0.68 \quad \text{Percent Composition of Iron} \]

\[ u_5 = \frac{u_{Fe}}{p_{Fe}} \times C_{Fe} \quad \text{Attenuation Coefficient for Iron} \]

\[ u_{Ni} = 3.28 \times 10^{-2} \quad \text{Mass Attenuation Coefficient for Nickel [cm}^2/\text{g]} \]

\[ p_{Ni} = 0.813 \quad \text{Density of Nickel [g/cc]} \]

\[ C_{Ni} = 0.1 \quad \text{Percent Composition of Nickel} \]

\[ u_6 = \frac{u_{Ni}}{p_{Ni}} \times C_{Ni} \quad \text{Attenuation Coefficient for Nickel} \]

\[ u_7 = u_2 + u_3 + u_4 + u_5 + u_6 \quad \text{Attenuation Coefficient for Stainless Steel} \]

\[ x = u_1 \times t_{Pb} + 2 \times u_7 \times t_{SS} \quad \text{Mean Free Path (mfp)} \]

\[ b = 1.48 \times 10^0 \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ c = 1.01 \times 10^0 \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ a = 1.2 \times 10^{-2} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ X = 1.31 \times 10^1 \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ d = -2.58 \times 10^{-2} \quad \text{Iron Exposure Buildup Factor from ANSI/ANS 6.4.3-1991} \]

\[ K = c \times x \times a + d \times \frac{((\text{tanh}(x/X)-2)-(\text{tanh}(-2)))/(1-\text{tanh}(-2))}{(1-\text{tanh}(-2))} \quad \text{Geometric Progression Approximation} \]

\[ B_E = 1 + (b-1) \times \frac{(K \times x - 1)}{(K - 1)} \quad \text{Build Up Factor} \]

\[ S_E = 1000000 \quad \text{Source [mrem/hr]} \]

\[ R = 2 \times t_{SS} + t_{Pb} \quad \text{total thickness of material and range to surface dose rate [cm]} \]

\[ \text{Dose}(S_E, B_E, x, R) \quad \text{Dose Rate [mrem/hr]} \]

\[ t_{Pb} = \]

<table>
<thead>
<tr>
<th>Columns 1 through 5</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.0600  0.0700  0.0800  0.0900  0.1000</td>
</tr>
</tbody>
</table>
Columns 6 through 10

0.1100  0.1200  0.1300  0.1400  0.1500

t_{SS} =
   9

u_{Pb} =
   0.0426

p_{Pb} =
   11.3500

C_{Pb} =
   1

u_{1} =
   0.0038

u_{Si} =
   0.0296

p_{Si} =
   0.0801

C_{Si} =
   0.0100

u_{2} =
   0.0037

u_{Cr} =
   0.0305

p_{Cr} =
   1.5224
\begin{align*}
C_{\text{Cr}} &= 0.1900 \\
u_3 &= 0.0038 \\
u_{\text{Mg}} &= 0.0304 \\
p_{\text{Mg}} &= 0.1663 \\
C_{\text{Mg}} &= 0.0200 \\
u_4 &= 0.0037 \\
u_{\text{Fe}} &= 0.0314 \\
p_{\text{Fe}} &= 5.4487 \\
C_{\text{Fe}} &= 0.6800 \\
u_5 &= 0.0039 \\
u_{\text{Ni}} &= 0.0328 \\
p_{\text{Ni}} &= 0.8130
\end{align*}
\[ C_{\text{Ni}} = 0.1000 \]
\[ u_6 = 0.0040 \]
\[ u_7 = 0.0191 \]
\[ x = \]
\[
\begin{array}{cccccc}
0.3442 & 0.3443 & 0.3443 & 0.3443 & 0.3444 \\
0.3444 & 0.3444 & 0.3445 & 0.3445 & 0.3446
\end{array}
\]
\[ b = 1.4800 \]
\[ c = 1.0100 \]
\[ a = 0.0120 \]
\[ X = 13.1000 \]
\[ d = -0.0258 \]
\[ K = \]
\[
\begin{array}{cccccc}
1.0104 & 1.0104 & 1.0104 & 1.0104 & 1.0104 \\
\end{array}
\]
Columns 6 through 10
    1.0104  1.0104  1.0104  1.0104  1.0104

B_E =

Columns 1 through 5
    1.1647  1.1647  1.1647  1.1647  1.1647

Columns 6 through 10
    1.1648  1.1648  1.1648  1.1648  1.1648

S_E =

    1000000

R =

Columns 1 through 5
    18.0600  18.0700  18.0800  18.0900  18.1000

Columns 6 through 10
    18.1100  18.1200  18.1300  18.1400  18.1500

ans =

Columns 1 through 5
    201.4009  201.1736  200.9466  200.7201  200.4939

Columns 6 through 10
    200.2681  200.0427  199.8177  199.5930  199.3687

>>
Iteration 61

%% Solve for Dose and truncate at 200 mrem/hr.

function [D] = Dose(t)

D = (1000000) .* (1 + (1.48 - 1) .* ((1.01) .* ((0.038) .* t + (0.019) * 18) .^ (0.012) + (0.0258) .* (((tanh(((0.038) .* t + (0.019) * 18) / 13.1) - 2) - (tanh(-2))) ./ (1 - tanh(-2)))) .^ ((0.038) .* t + (0.019) .* 18) - 1) ./ ((1.01) .* ((0.038) .* t + (0.019) .* 18) .^ (0.012) + (0.0258) .* (((tanh(((0.038) .* t + (0.019) * 18) / 13.1) - 2) - (tanh(-2))) ./ (1 - tanh(-2)))) - 1)) .* exp(-((0.038) .* t + (0.019) .* 18)) ./ (4 * pi .* (18 + t) .^ 2);

x= .1756

%% Shielding at 5 MeV

%% Source at 1,000,000 mrem/hr

%% t_SS = 9 cm

t= [0.12:0.0001:0.14]

t =

Columns 1 through 5
0.1200 0.1201 0.1202 0.1203 0.1204

Columns 6 through 10
0.1205 0.1206 0.1207 0.1208 0.1209

Columns 11 through 15
0.1210 0.1211 0.1212 0.1213 0.1214

Columns 16 through 20
0.1215 0.1216 0.1217 0.1218 0.1219

Columns 21 through 25
0.1220 0.1221 0.1222 0.1223 0.1224

Columns 26 through 30
0.1225 0.1226 0.1227 0.1228 0.1229
<table>
<thead>
<tr>
<th>Columns 31 through 35</th>
</tr>
</thead>
<tbody>
<tr>
<td>0.1230   0.1231   0.1232   0.1233   0.1234</td>
</tr>
<tr>
<td>Columns 36 through 40</td>
</tr>
<tr>
<td>0.1235   0.1236   0.1237   0.1238   0.1239</td>
</tr>
<tr>
<td>Columns 41 through 45</td>
</tr>
<tr>
<td>0.1240   0.1241   0.1242   0.1243   0.1244</td>
</tr>
<tr>
<td>Columns 46 through 50</td>
</tr>
<tr>
<td>0.1245   0.1246   0.1247   0.1248   0.1249</td>
</tr>
<tr>
<td>Columns 51 through 55</td>
</tr>
<tr>
<td>0.1250   0.1251   0.1252   0.1253   0.1254</td>
</tr>
<tr>
<td>Columns 56 through 60</td>
</tr>
<tr>
<td>0.1255   0.1256   0.1257   0.1258   0.1259</td>
</tr>
<tr>
<td>Columns 61 through 65</td>
</tr>
<tr>
<td>0.1260   0.1261   0.1262   0.1263   0.1264</td>
</tr>
<tr>
<td>Columns 66 through 70</td>
</tr>
<tr>
<td>0.1265   0.1266   0.1267   0.1268   0.1269</td>
</tr>
<tr>
<td>Columns 71 through 75</td>
</tr>
<tr>
<td>0.1270   0.1271   0.1272   0.1273   0.1274</td>
</tr>
<tr>
<td>Columns 76 through 80</td>
</tr>
<tr>
<td>0.1275   0.1276   0.1277   0.1278   0.1279</td>
</tr>
<tr>
<td>Columns 81 through 85</td>
</tr>
<tr>
<td>0.1280   0.1281   0.1282   0.1283   0.1284</td>
</tr>
<tr>
<td>Columns 86 through 90</td>
</tr>
<tr>
<td>0.1285   0.1286   0.1287   0.1288   0.1289</td>
</tr>
<tr>
<td>Columns 91 through 95</td>
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<td>----------------------</td>
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<tr>
<td>Columns 96 through 100</td>
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<tr>
<td>Columns 101 through 105</td>
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<td>Columns 106 through 110</td>
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<td>Columns 111 through 115</td>
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<td>Columns 116 through 120</td>
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<td>Columns 126 through 130</td>
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<td>Columns 131 through 135</td>
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<td>Columns 136 through 140</td>
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<td>Columns 141 through 145</td>
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<td>Columns 146 through 150</td>
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<tr>
<td>Columns 151 through 155</td>
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<td>------------------------</td>
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<td>Columns 156 through 160</td>
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<td>Columns 161 through 165</td>
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</tr>
<tr>
<td>Columns 166 through 170</td>
</tr>
<tr>
<td>0.1365</td>
</tr>
<tr>
<td>Columns 171 through 175</td>
</tr>
<tr>
<td>0.1370</td>
</tr>
<tr>
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<tr>
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</tr>
<tr>
<td>Columns 181 through 185</td>
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<tr>
<td>0.1380</td>
</tr>
<tr>
<td>Columns 186 through 190</td>
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<tr>
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<tr>
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<tr>
<td>Columns 196 through 200</td>
</tr>
<tr>
<td>0.1395</td>
</tr>
<tr>
<td>Column 201</td>
</tr>
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</table>
Dose(t)

ans_1 =

Columns 1 through 5
200.0415  200.0389  200.0362  200.0336  200.0309

Columns 6 through 10
200.0282  200.0256  200.0229  200.0203  200.0176

Columns 11 through 15
200.0150  200.0123  200.0097  200.0070  200.0043

Columns 16 through 20
200.0017  199.9990  199.9964  199.9937  199.9911

Columns 21 through 25
199.9884  199.9858  199.9831  199.9804  199.9778

Columns 26 through 30
199.9751  199.9725  199.9698  199.9672  199.9645

Columns 31 through 35
199.9619  199.9592  199.9566  199.9539  199.9512

Columns 36 through 40
199.9486  199.9459  199.9433  199.9406  199.9380

Columns 41 through 45
199.9353  199.9327  199.9300  199.9274  199.9247

Columns 46 through 50
199.9220  199.9194  199.9167  199.9141  199.9114

Columns 51 through 55
199.9088  199.9061  199.9035  199.9008  199.8982
Columns 56 through 60
199.8955  199.8902  199.8875  199.8849

Columns 61 through 65
199.8822  199.8796  199.8769  199.8743  199.8716

Columns 66 through 70
199.8690  199.8663  199.8637  199.8610  199.8584

Columns 71 through 75
199.8557  199.8531  199.8504  199.8478  199.8451

Columns 76 through 80
199.8424  199.8398  199.8371  199.8345  199.8318

Columns 81 through 85
199.8292  199.8265  199.8239  199.8212  199.8186

Columns 86 through 90
199.8159  199.8133  199.8106  199.8080  199.8053

Columns 91 through 95
199.8027  199.8000  199.7974  199.7947  199.7921

Columns 96 through 100
199.7894  199.7868  199.7841  199.7815  199.7788

Columns 101 through 105
199.7762  199.7735  199.7708  199.7682  199.7655

Columns 106 through 110
199.7629  199.7602  199.7576  199.7549  199.7523

Columns 111 through 115
199.7496  199.7470  199.7443  199.7417  199.7390
<table>
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<td>Columns 121 through 125</td>
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<tr>
<td>Columns 126 through 130</td>
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<tr>
<td>Columns 131 through 135</td>
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<tr>
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<tr>
<td>Columns 136 through 140</td>
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<tr>
<td>Columns 141 through 145</td>
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<tr>
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</tr>
<tr>
<td>Columns 146 through 150</td>
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<tr>
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</tr>
<tr>
<td>Columns 156 through 160</td>
</tr>
<tr>
<td>199.6304  199.6277  199.6251  199.6225  199.6198</td>
</tr>
<tr>
<td>Columns 161 through 165</td>
</tr>
<tr>
<td>199.6172  199.6145  199.6119  199.6092  199.6066</td>
</tr>
<tr>
<td>Columns 166 through 170</td>
</tr>
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<td>199.6039  199.6013  199.5986  199.5960  199.5933</td>
</tr>
<tr>
<td>Columns 171 through 175</td>
</tr>
<tr>
<td>199.5907  199.5880  199.5854  199.5827  199.5801</td>
</tr>
</tbody>
</table>
Columns 176 through 180
199.5774  199.5748  199.5721  199.5695  199.5668
Columns 181 through 185
199.5642  199.5615  199.5589  199.5563  199.5536
Columns 186 through 190
199.5510  199.5483  199.5457  199.5430  199.5404
Columns 191 through 195
199.5377  199.5351  199.5324  199.5298  199.5271
Columns 196 through 200
199.5245  199.5218  199.5192  199.5165  199.5139
Column 201
199.5113

find(ans<200)

ans =
Columns 1 through 9
17  18  19  20  21  22  23  24  25
Columns 10 through 18
26  27  28  29  30  31  32  33  34
Columns 19 through 27
35  36  37  38  39  40  41  42  43
Columns 28 through 36
44  45  46  47  48  49  50  51  52
Columns 37 through 45
53  54  55  56  57  58  59  60  61
\text{min(ans)}
\begin{align*}
\text{ans}_2 & = 17 \\
\text{t(17)} & \\
\text{ans}_3 & = 0.1216 \\
\text{ans}_4(17) & = 199.9990
\end{align*}
APPENDIX B: MATLAB OPTIMIZATION CODING

The optimization technique used in Matlab was to provide a more concise solution to the shielding calculation formula for the Clamshell Cask. The process used was to set the formula equal to zero, then optimize the solution with x and y resembling the Lead thickness and Stainless Steel thickness, respectively. The following was the formula used:

```matlab
>>f = @(x,y) ((1000000) .* (1 + (1.48 - 1) .* ((((1.01) .* ((0.038) .* x + (0.019) .* 2.*y) ^ (0.012) + (0.0258) .* (((tanh(((0.038) .* x + (0.019) .* 2.*y) ./ 13.1) - 2) - (tanh(-2))) ./ (1-tanh(-2)))) .^ ((0.038) .* x + (0.019) .* 2.*y) - 1) ./ ( ((1.01) .* ((0.038) .* x + (0.019) .* 2.*y) - 1) ./ ( ((1.01) .* ((0.038) .* x + (0.019) .* 2.*y) - 1) ./ (1-tanh(-2)))) .^ (0.012) + (0.0258) .* ((tanh(((0.038) .* x + (0.019) .* 2.*y) ./ 13.1) - 2) - (tanh(-2))) ./ (1 - tanh(-2)))) - 1)) .* exp(-(0.038) .* x + (0.019) .* 2.*y) ./ (4 .* pi .* (2.*y + x) .^ 2))^200;
```

The formula was then modeled against the two materials’ thicknesses so as to establish the range for which the optimization local minimum exists.

```matlab
>>fsurf (f,[0,10],showcontours,'on');
```
APPENDIX C: ACRONYMS

AIS – Air Intake Shaft
C.F.R – Code of Federal Regulation
CH – Contact Handled
cm – Centimeters
DHLW – Defense High Level Waste
DOE – Department of Energy
DSA – Design Safety Analysis
EPA – Environmental Protection Agency
ES – Exhaust Shaft
Ev – Electron Volt
HAC – Hazardous Accident Condition
HEM – Horizontal Emplacement Machine
HLW – High Level Waste
HRA – High Radiation Area
HWFP – Hazardous Waste Facility Permit
in – Inch
in3 – Cubic Inches
lb – Pound
LHD – Load Haul Dump
LWA – Land Withdrawal Act
Matlab – Matrix Laboratory
MeV – Mega Electron Volt
mfp – Mean Free Path
mrem/hr – Millirem per Hour
NMED – New Mexico Environmental Department
RCRA – Resource Conservation and Recovery Act
RH – Remote Handled
ROM – Run of Mine
ROV – Remotely Operated Vehicle
SDDI – Salt Defense Disposal Investigations
SAR – Safety Analysis Report
SEIS – Supplemental Environmental Impact Statement
SHS – Salt Handling Shaft
TRAMPAC – TRU Waste Authorized Methods for Payload Control
TRU – Transuranic
TRUPACT – Transuranic Packaging Transporter
TRUDOCK – TRUPACT II Unloading Dock
UG – Underground
WAC – Waste Acceptance Criteria
WCS – Waste Control Specialist
WHB – Waste Handling Building
WHS – Waste Hoist Shaft
REFERENCES


DOE/WIPP-07-3372, the WIPP Design Safety Analysis, Revision 5. May 2016.


The CH-TRAMPAC, Revision 4. April 2012.

The RH-TRAMPAC, Revision 0. June 2006.


